

IN THE CLAIMS:

Claims 1-4. (Cancelled)

5. (Withdrawn) A process for preparing modified polypropylene (A2), comprising melt kneading polypropylene (B2) and a peroxydicarbonate (C) using an extruder at a temperature of 170 to 250°C in such a manner that the specific energy (E_{SP}) becomes 0.25 to 0.8 kW hr/kg to prepare modified polypropylene (A2) having a melt flow rate (ASTM D1238, 230°C, load of 2.16 kg) of 0.1 to 10 g/10 min, a melt tension of 3 to 20 g and a gel fraction, as determined by boiling paraxylene extraction, of 0.01 to 25 % by weight.

6. (Withdrawn) The process for preparing modified polypropylene (A2) as claimed in claim 5, wherein the extruder is a twin-screw extruder.

7. (Withdrawn) The process for preparing modified polypropylene (A2) as claimed in claim 6, wherein at least one kneading section is provided in the screw arrangement of the twin-screw extruder.

8. (Original) The process for preparing modified polypropylene (A2) as claimed in any one of claims 5 to 7, wherein the peroxydicarbonate (C) is bis(4-t-butylcyclohexyl)peroxydicarbonate.

9. (Withdrawn) The process for preparing modified polypropylene (A2) as claimed in any one of claims 5 to 7, wherein the peroxydicarbonate (C) is dicetyl peroxydicarbonate.

10. (Withdrawn) A process for preparing modified polypropylene (A3), comprising melt kneading polypropylene (B1), a polypropylene crosslinking type peroxide (D) and a polypropylene decomposition type peroxide (E) at a temperature of 160 to 250°C.

11. (Withdrawn) The process for preparing modified polypropylene (A3) as claimed in claim 10, wherein the polypropylene crosslinking type peroxide (D) is a peroxydicarbonate.

12. (Withdrawn) The process for preparing modified polypropylene (A3) as claimed in claim 11, wherein the peroxydicarbonate is bis(4-t-butylcyclohexyl) peroxydicarbonate.

13. (Withdrawn) The process for preparing modified polypropylene (A3) as claimed in claim 11, wherein the peroxydicarbonate is dicetyl peroxydicarbonate.

14. (Withdrawn) The process for preparing modified polypropylene (A3) as claimed in any one of claims 10 to 13, wherein the polypropylene decomposition type peroxide (E) is a dialkyl peroxide.

15. (Withdrawn) The process for preparing modified polypropylene (A3) as claimed in claim 14, wherein the dialkyl peroxide is 2,5-dimethyl-2,5-bis(t-butyperoxy)hexane.

16. (Withdrawn) A process for preparing modified polypropylene (A4), comprising melt kneading polypropylene (B1) and a polypropylene crosslinking type peroxide (D) at a temperature of 160 to 250°C and then melt kneading the resulting

kneadate and a polypropylene decomposition type peroxide (E) at a temperature of 160 to 250°C.

17. (Withdrawn) The process for preparing modified polypropylene (A4) as claimed in claim 16, wherein the polypropylene crosslinking type peroxide (D) is a peroxydicarbonate.

18. (Withdrawn) The process for preparing modified polypropylene (A4) as claimed in claim 17, wherein the peroxydicarbonate is bis(4-t-butylcyclohexyl)peroxydicarbonate.

19. (Withdrawn) The process for preparing modified polypropylene (A4) as claimed in claim 17, wherein the peroxydicarbonate is dicetyl peroxydicarbonate.

20. (Withdrawn) The process for preparing modified polypropylene (A4) as claimed in any one of claims 16 to 19, wherein the polypropylene decomposition type peroxide (E) is a dialkyl peroxide.

21. (Withdrawn) The process for preparing modified polypropylene (A4) as claimed in claim 20, wherein the dialkyl peroxide is 2,5-dimethyl-2,5-bis(t-butylperoxy)hexane.

22. (Previously Presented) A modified polypropylene composition (F1) comprising:

(B3) polypropylene, and

(A1) a modified polypropylene having a melt flow rate (ASTM D1238, 230°C, load of 2.16 kg) of 0.1 to 10 g/10 min, a melt tension of 3 to 20 g and a gel fraction, as determined by boiling paraxylene extraction, of 0.01 to 25 % by weight, wherein the polypropylene (B3) is contained in an amount of 1 to 50 % by weight and the modified polypropylene (A1) is contained in an amount of 50 to 99 % by weight, the total of said components (A1) and (B3) being 100 % by weight.

Claims 23-25. (Cancelled)

26. (Withdrawn) A foamed product obtained from the modified polypropylene (A3) prepared by the process of claim 10.

27. (Withdrawn) A foamed product obtained from the modified polypropylene (A4) prepared by the process of claim 16.

28. (Original) A foamed product obtained from the modified polypropylene composition (F1) of claim 22.

29. (Cancelled)

30. (Previously Presented) The modified polypropylene composition (F1) as claimed in claim 22, wherein the modified polypropylene (A1) is obtained by melt kneading 98.5 to 99.7 % by weight of polypropylene (B1) having a melt flow rate of 0.4 to 15 g/10 min and 0.3 to 1.5 % by weight of a peroxydicarbonate (C) at a temperature of 170 to 250°C.

31. (Previously Presented) The modified polypropylene composition (F1) as claimed in claim 30, wherein the peroxydicarbonate (C) is bis(4-t-butylcyclohexyl) peroxydicarbonate.

32. (Previously Presented) The modified polypropylene composition (F1) as claimed in claim 30, wherein the peroxydicarbonate (C) is dicetyl peroxydicarbonate.

Claims 33-36. (Cancelled)

37. (Previously Presented) The modified polypropylene composition (F1) as claimed in claim 22, wherein the polypropylene (B3) is contained in an amount of 5 to 20 % by weight, the total of said components (A1) and (B3) being 100 % by weight.

38. (Previously Presented) The modified polypropylene composition (F1) as claimed in claim 22, wherein the modified polypropylene (A1) is contained in an amount of 80 to 95 % by weight, the total of said components (A1) and (B3) being 100 % by weight.

39. (Previously Presented) The modified polypropylene composition (F1) as claimed in claim 22, wherein the polypropylene (B3) is contained in an amount of 5 to 20 % by weight and the modified polypropylene (A1) is contained in an amount of 80 to 95 %

by weight, the total of said components (A1) and (B3) being 100 % by weight.